

In-situ synchrotron x-ray radiography investigations of water transport in PEM fuel cells

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Abstract

Water transport in an operating PEM fuel cell was investigated with synchrotron x-ray radiography with a spatial resolution of 3 μm and a temporal resolution of 5 seconds. This method allows for the detection of water accumulations with less than 10 μm diameter. We demonstrate that synchrotron x-ray imaging can dramatically expand the possibilities of imaging with high spatial and time resolution, especially as a complement to neutron radiography. Water transport processes from the first appearance of small water accumulations in the gas diffusion layer to their transport into the channel system were analyzed in situ. Correlations between local effects such as water formation and operating conditions of the whole system, e.g. power variations, were found. A recently described eruptive water transport mechanism is analyzed in detail.

Key words: fuel cell, synchrotron x-ray radiography, imaging, water transport, two-phase flow, gas diffusion layer

1 Introduction

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During the past decade, the global demand for energy has exploded, raising the need for highly efficient energy conversion that combines with new technologies to satisfy the need for safe energy supplies [1-3]. Fuel cell technology has the advantage of directly converting chemical energy into electrical and thermal energy without noise or hazardous emissions and contributes to a safe, sustainable energy supply.

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Low temperature polymer electrolyte (PEM) fuel cells are the most promising candidates for future applications in mobile and stationary applications [1-3]. In PEM fuel cells, hydrogen and oxygen react to form water and, due to the separation of the anodic and cathodic processes, electrical energy. Protons migrate through the membrane and recombine with oxygen on the surface of the cathodic catalyst where oxygen is reduced and forms water (see schematic drawing of a typical cross section through a PEM fuel cell in Fig. 1).

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In PEM fuel cells, liquid water plays a crucial role. On the one hand, only the wet membrane is proton conductive; a dry polymer membrane changes its structure and the conductivity of the membrane collapses. On the other hand, flooding is a significant source of power losses during fuel cell operation [1-5]. If the catalyst layer and the adjacent gas diffusion layer are filled with liquid water, the transport of reactant and product gases (O_2 , H_2 and H_2O) is strongly hindered and the supply of the reactive area, i.e. the catalyst, is reduced. Thus a well-balanced water management, i.e. wet conditions coupled with simultaneous fast transport of product water, at any operating condition is an important aspect of development and, along with the choice of the membrane materials, a major challenge for the efficiency and lifetime of PEM fuel cells [6].

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In the past few years, interest in these issues has been increasing continuously and many advances have been made in this field. However, a complete insight into the fundamental processes of liquid water development and transport is still missing, hampering a specific strategy for component development.

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5 Besides the flow field and membrane, the GDL is the most important
6 component as it is responsible for wetting the membrane as well as for the fast
7 transfer of liquid water from the catalyst to the flow field channel. The most
8 commonly used GDL materials consist of carbon fibers that are a few μm thick
9 and are more or less arbitrarily distributed. This results in typical porosities of
10 60-80% with pore sizes of a few 10 μm in diameter. The carbon fibers are
11 normally coated with a hydrophobic material such as teflon in order to prevent
12 the development of a thin film of liquid water at the catalyst. The structure of a
13 sophisticated GDL material can be very complex and varies depending on the
14 required properties for the corresponding fuel cell. However, the high complexity
15 of the interaction between environmental conditions inside a fuel cell and
16 materials properties do not allow for a sufficiently detailed prediction of water
17 development and transport. Development of advanced models that describe the
18 water transport under any operating condition is therefore desirable. For this
19 task it is essential to obtain insights into the fundamental mechanisms of water
20 transport in the GDL pore network that act as a channel system for the flowing
21 liquid water.
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36 Although progresses in water transport simulations were achieved [7-23], until
37 now only a few techniques for in-situ investigations have been available.
38 Preparation of special fuel cell setups, e.g. with optically transparent
39 components, is possible [24-26] but introduces distortions into the system and
40 provides only limited access to the water transport inside the GDL which is not
41 transparent. In the past, neutron radiography has been found to be very useful
42 for in-situ investigations of the transport of water in the flowfields and the water
43 saturation in the GDLs [27-41]. The high penetration depths into many materials
44 – especially metals – and the comparable high attenuation coefficient of
45 hydrogen makes neutron imaging an excellent technique for investigation of the
46 distribution of hydrogen-containing materials, e.g. behind metallic components
47 [42,43], in general. For investigations of small fuel cells magnetic resonance
48 imaging was applied very successfully [44-46].
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One of the main drawbacks of neutron imaging is the rather low spatial resolution of typically 100-250 μm [42]. Recent achievements in detector development enable spatial resolutions down to about 20-50 μm [36,37]. However, the rather low neutron flux of less than $10^6\text{mm}^{-2}\text{s}^{-1}$ available even at the best neutron sources limits the signal-to-noise ratio and makes long exposure times of typically 5-30 min necessary for high resolution measurements. This is not sufficient for fast investigations of the water formation and transport dynamics in the small pores of the GDL or the transition step of water from the GDL to the channel. Even if the spatial resolution is very close to the typical pore sizes of around 10 μm to 50 μm , a time resolution of a few seconds is not achievable.

Imaging instruments at synchrotron x-ray sources do not have these limitations. They are very suitable for investigations of small areas (around a few mm) with a spatial resolution of a few μm . The comparable high x-ray flux, typically between 10^{10} and 10^{12} photons/(mm^2s) and sometimes more depending on the instrument setup, provides sufficient signal-to-noise-ratio even at short exposure times of a few seconds. However, x-rays are strongly attenuated by metals and other components used in fuel cells.

In this paper investigations on the water transport behavior in the GDL of an operating fuel cell are shown. A spatial resolution of 3 μm and a time resolution of 5 s were achieved by using synchrotron x-ray radiography. Both the resolution and the ability to perform measurements in an (almost) unmodified and undisturbed system exhibit a unique method to gain a realistic image of the transport and production of liquid water [47, 48].

2 Experimental setup

2.1 Synchrotron x-ray imaging facility

The experiments were performed at the tomography facility of the Helmholtz Centre Berlin (formerly Hahn-Meitner Institute Berlin) and the Federal Institute of Materials Research and Testing (BAM), the BAMline, which is located at the synchrotron source BESSY in Berlin (Germany) [49]. A W-Si

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multilayer monochromator with an energy resolution of about $\Delta E/E = 10^{-2}$ was used to obtain a monochromatic x-ray beam with an energy of 13 keV. This energy was chosen to provide good transmission through the prepared fuel cell (for details see below) while maintaining sufficient sensitivity to water, i.e. the reduction in transmission by the water is strong enough to visualize it without the use of any contrast medium despite the strong absorption of the other fuel cell components. A 2048x2048 pixel² camera setup (Princeton VersArray 2048B with a Gadox scintillator screen) was used to capture image area sizes up to 7x7 mm² with pixel sizes between 1.5 and 3.5 μm and a physical spatial resolution of typically 3-8 μm . The measurement time per image was around 4.8 s, consisting of 1 s exposure time and 3.8 s read-out time. In this way, a good compromise between measurement time and signal-to-noise ratio was achieved. A schematic drawing of the radiography setup is shown in Fig. 2.

The fuel cell was mounted on translation and rotation stages. In this way, the region of interest could be selected and the cell could also be driven to the side for the measurement of flat field images, which are taken to eliminate inhomogeneities in the beam intensity distribution. In the normalization step, all radiographic images are divided by a corresponding flat field image.

2.2 Fuel cells

A single cell setup was used for all measurements; the anodic and cathodic threefold serpentine flow fields with 1 mm wide channels and ribs and an active area of 100 cm² were machined in separate blank graphite composite plates (SGL Carbon) with the cooling water distribution field grafted into the cathodic part. GORE PRIMEA 5620 membrane electrode assemblies with a platinum loading of 0.3 mg/cm² on the anode and 0.4 mg/cm² on the cathode side were employed [50]. SGL Carbon 10 BB material was used as the GDL [50]. The operating cell was investigated through small holes of 8 mm diameter in the metallic end-plates of the cell that were carefully sealed. Liquid water from the cooling bypassed these positions. The flow field and the other components remained completely unmodified. Thus, the slight modification of

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the housing does not influence the thermal and electrical conductivity of the components and the water development and transport in the cell.

3 Experimental results

A typical raw image as obtained during the experiment is shown in Fig. 3a. The flow field channels on the cathode and anode side can be seen. The best way to derive the water distribution from this image is normalization with respect to a radiogram of a “dry” cell. This way, the pure liquid water distribution is obtained (Fig. 3b). The white spots in the image can be assigned to water clusters in GDL material and flow field channels (white arrows). In most cases, the image used for normalization is not completely “dry” - a few water droplets might remain in the GDL or even the channels. These can be identified as black areas in this image (black arrows). The reason for this is that the initial image of a dry cell cannot always be used for all measurements due to mechanical creep and thermal expansion of the setup which slightly changes the location of the cell. These effects make it impossible to keep the setup at a constant position within the required accuracy of around 1 μm for long periods of time. In the example shown in Fig. 3b, a large (around 1 mm diameter) water droplet was located in the anodic flow field channel and was removed after the fuel cell was started again causing “negative” water accumulations in the normalized radiogram. “Negative” means in this context that there is less water at this specific location in an operating cell than in the “dry” cell.

Figure 4 compares neutron and synchrotron x-ray radiography for fuel cell research in order to demonstrate the complementarity of the techniques. Neutron radiography is able to map the whole active area of the cell in the order of 100 to 200 cm^2 . The metallic and carbon components can be penetrated by the neutrons at all locations. On the other side, synchrotron x-ray radiography is employed to investigate one part of the cell with very high spatial resolution.

Since the advantages of neutron imaging are well known, we would like to demonstrate the specific strengths of synchrotron x-ray radiography in more

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5 detail. Figure 5 shows a comparison of the achievable spatial resolution
6 between synchrotron x-ray and neutron radiography. All images were taken
7 from the same area of the same fuel cell. The exposure time was 1 s for the
8 synchrotron x-ray radiographic images and 10 s for the neutron radiographic
9 images. Read-out time was 3.8 s in both cases. Although at long exposure
10 times of around a few minutes image quality is excellent and important
11 information about the saturation of the GDL and its distribution can be obtained
12 [36,37], a detailed analysis of the exact water formation in the GDL pores and
13 the correlated fast transport processes within the GDL is a challenge normally
14 beyond the potential of neutron imaging. This can be derived from the neutron
15 radiography image shown in Fig. 5a), which was taken with an exposure time of
16 only 10 s: Some small droplets in the channels can be seen and the overall
17 saturation in the GDL might be derived from the image. However, it is practically
18 impossible to see the small water accumulations in the GDL pores. Although a
19 maximum achievable spatial resolution of around 70 μm was possible with this
20 setup the modulation transfer function gives a spatial resolution in the range of
21 around 150 μm in the shown image caused by the limited count rate due to the
22 short exposure time. The rather low spatial resolution is mainly caused by the
23 weak signal and correlated low signal-to-noise ratio in fast measurements.
24 Image quality cannot be further increased by increasing the spatial resolution.

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26 This image is now compared to a synchrotron x-ray radiogram in Fig 5b.
27 Enlargements of the areas marked in black in Fig. 5 a and b are displayed in
28 Fig. 5 c and d, respectively. The differences between neutron and synchrotron
29 x-ray radiography are obvious. In the synchrotron x-ray radiograms the water
30 droplets are displayed with such a high accuracy that even details like the
31 droplets' contact angle at the channel-material surface and the droplets'
32 orientation in space can be determined. In addition, fine water accumulations in
33 the GDL pores with only a few μm in diameter can be seen [see arrows in Fig. 5
34 d)]. This comparison clearly demonstrates the advantage of synchrotron x-ray
35 radiography for fast and high resolution measurements.

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37 It should be mentioned that this method also has its limitations: if, for example,
38 some metallic components such as a metal flow field are in the line of the beam
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5 the low x-ray energy used here is not sufficient to penetrate the fuel cell. On the
6 other hand, at higher x-ray energies, where metals can be penetrated easily,
7 the attenuation of water is too small; limitations in the signal to noise ratio then
8 prevent the clear visualization of water. The following investigations
9 demonstrate the high potential of synchrotron x-ray radiography for visualization
10 of water clusters in GDL materials.
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15 Fig. 6 a) shows the evolution of liquid water accumulations in the GDL.
16 Additionally, an enlargement of the area marked in white is given in Fig. 6 b).
17 The fuel cell was started at almost dry condition. The time interval between the
18 images was 81.6 s, after which some water accumulations in the GDL appear.
19 These first accumulations start beneath the land (rib) of the flow field. These
20 initial spots of liquid water formation are located beneath the land (ribs) of the
21 flow field. Hardly any water can be seen in the GDL beneath the channel.
22 However, inside the channels a few water droplets can be found at the channel
23 edges. After 2 x 81.6 s the size and amount of the water accumulations
24 increased. After about 10 min. (7 x 81.6s) almost stationary conditions – near
25 equilibrium – are reached and the water saturation does not increase any more.
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36 Along the black rectangle in Fig. 6a (image at the bottom right) horizontal cross
37 sections were taken (approx. 100 horizontal lines were summed up) and the
38 intensities are displayed as line graphs in Fig. 7. As mentioned above, water
39 accumulates first in the GDL below the land. Inside the channel, only a few
40 water droplets at the side of the flow field channels were found.
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46 An interesting feature is the fast droplet building in the flow field channel. The
47 white arrows in Fig. 6a mark the position of such a droplet formation event in
48 the flowfield channel. These processes do not occur completely arbitrarily, but
49 have a specific repetition rate that is correlated with the operating conditions of
50 the fuel cell. This will be shown in the next example where the water transport
51 behavior on a much shorter time scale is investigated.
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56 Figure 8a shows again the same area in the fuel cell, but with smaller time
57 steps of 4.8 s (the time resolution). At first, water has accumulated in the GDL
58 pores (black spots disappear while more white spots appear). After the
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4 accumulation reached a specific level, the water was expelled into the channels
5 where it formed two droplets (white arrows). As can be seen, the droplet
6 formation occurs from one image to the other within a time interval below the
7 time resolution of 4.8 s. The droplets evaporate within the next 10-15 s. A 100%
8 relative humidity has not been reached and the droplets can evaporate.
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11 Fig. 9 shows a schematic drawing of this eruptive transport. Firstly, water
12 accumulates in the pores of the GDL until a specific amount is reached. Then,
13 within a few seconds or even less, one part of the water is expelled and forms a
14 droplet at the channel wall.
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17 The whole sequence of Fig. 8a repeats again after some time is passed. The
18 process is periodic with an almost constant period time. This is demonstrated in
19 Fig. 8b. This image series shows the same location 105.6 s later. It is
20 remarkable that the images are almost identical to those in Fig. 8a. The overall
21 periodicity is kept during the entire observation time of more than 45 min. This
22 water transport mechanism is very sensitive to changes in the operating
23 parameters as will be shown in the next example.
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26 The image series in Fig. 10 was taken during transition from one operating
27 condition to another. The series shows one of the eruptive water transport
28 channels with time intervals of 4.8 s between succeeding images. Each eruptive
29 event is marked by a white arrow. At the beginning of this series, specific
30 operating conditions have been set ($u_C=25\%$, $u_A=95\%$, $i_0=500 \text{ mA/cm}^2$) from
31 which one of the parameters – the anodic utilization rate u_A – was slightly
32 changed from 95 % to 97.5 %. The system needs some time before changes in
33 the operating parameters affect the water transport behavior as can be derived
34 from Fig. 10. At first, the repetition time of the eruption cycle was about $40 \pm 5 \text{ s}$.
35 After around 200 s (40 images), the repetition time decreases slowly to about
36 $25 \pm 5 \text{ s}$.
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39 In addition, the water eruption behavior was altered. Beginning from the cycle
40 marked by a white circle, the droplet does not appear immediately with
41 maximum size but seems to grow over a time scale of around 10s to 15 s. Then
42 it disappears suddenly. The time scale of only about 5 s seems to be too small
43 for droplet evaporation. It is possible that the droplet size increases to a specific
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4 level where the resistance of the air flow is high enough to drive it away.
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6 Alternatively, another droplet wandering through the channel could be the
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8 reason (“avalanche” effect).
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10 After about 230 s, a very interesting new effect is observed: a second “transport
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12 channel” opens (black arrow) just below the old one and changes the overall
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14 water transport behavior, a detailed discussion will be given below.

15 The periodic behavior of the water droplet eruption (Fig. 8 and 10) can be well
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17 illustrated by monitoring the local water thickness at the droplet’s position as a
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19 function of time as shown in Fig. 11[a) and b). Each up and down sequence
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21 marks an entire cycle of water expulsion into the channel with subsequent
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23 evaporation of the water droplet.

24 The correlation between the water droplet formation in the channel and water
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26 agglomerations in the GDL is illustrated in Fig.11 c), where the local water
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28 thickness at the marked location in the GDL (see black arrows) was monitored.
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30 For comparison, the corresponding water thickness at the droplet position is
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32 shown as well and reveals the strong correlation: period times are identical and
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34 the water thickness in the GDL is reduced once a droplet in the channel evolves
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36 at the same time.
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38 **4 Discussion**

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40 The observation of the first appearance of water clusters beneath the lands
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42 (ribs) of the flow field is in accordance with theoretical predictions, for example
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44 by Kulikovskiy et al. [51]. The effect can be explained by an interplay of several
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46 factors as, e.g., compression of the GDL below the land, leading to a reduced
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48 porosity and extended pathway lengths for product and reactant gases.

49 The observations concerning the eruptive water transport mechanism is in
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51 agreement with the recent findings by Djilali et al. [52-55], who used fluorescent
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53 imaging to follow the water transport in GDL materials. They found quick
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55 ejection of droplets from the GDL very similar to to the findings here. The
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57 observation can be explained as follows: water is transported through the paths
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59 with least resistance. Due to inhomogenities in the GDL, surface water emerges
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at preferential locations, e.g. locations with a comparatively large hole in the

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fiber network. It should also be mentioned that Owejan et al. found hints for an eruptive water transport using neutron radiography [41].

The opening of a new “transport channel” as indicated in Fig. 10 (green arrow) could be explained by changes in the pressure distribution within the water-filled GDL due to the changed operating parameters [53]. The amount of liquid water produced in the cell strongly depends on several parameters such as the current density i_0 and the utilization rates. A similar observation was also described very recently by Bazilak et al. in ex-situ studies [53]. They found that the process of the building of breakthrough locations is dynamical. For example, they observed that forming a new breakthrough location could cause the old breakthrough location to recede. These findings are now supported by our in-situ investigations.

5 Conclusions

We demonstrated the strength of synchrotron x-ray radiography to study liquid water transport in fuel cells with a high level of detail. Compared to neutron radiography, only a rather small area can be investigated and slight modifications have to be made to the cell. However, synchrotron x-ray radiography represents the only technique for investigations of fast water transport phenomena in the pores of the GDL materials of fuel cells. Thus water accumulations less than 10 μm in diameter were visualized in-situ. In addition, fast processes such as the “eruptive” water droplet expulsion from the GDL into the flow field channels were studied and could help to understand the underlying water transport mechanisms.

Based on these findings, by synchrotron x-ray radiography the development of sophisticated GDL materials and flow fields as well as water transport models in fuel cell research can be significantly affected. In future, spatial and time resolution might be enhanced by at least one order of magnitude. The applied technique opens a variety of possibilities for future material optimization and might serve as basis for simulation purposes.

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34 experimental setup and procedure. In no case does such an identification imply
35 recommendation or endorsement nor does it imply that these materials are necessarily
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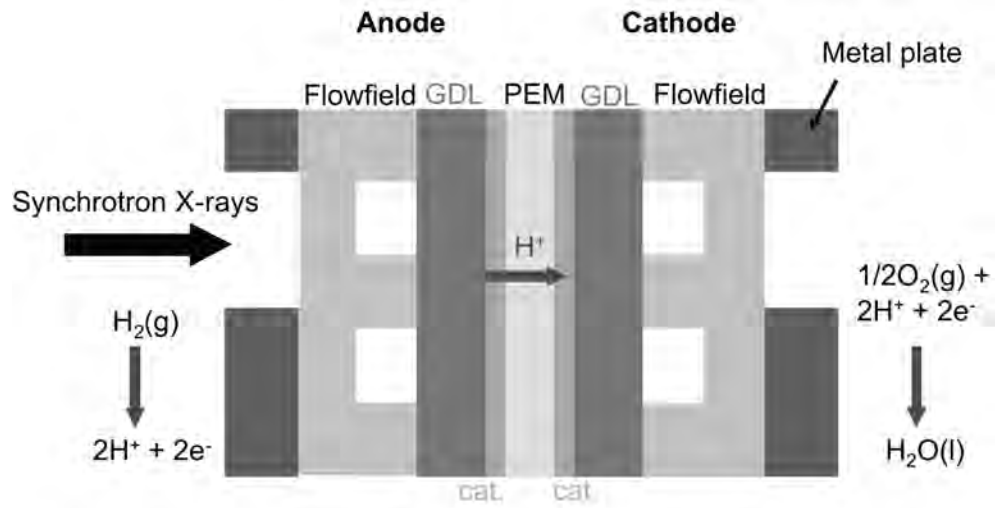


Fig. 1: Schematic drawing of a typical cross-section through a PEM fuel cell.
85x44mm (600 x 600 DPI)

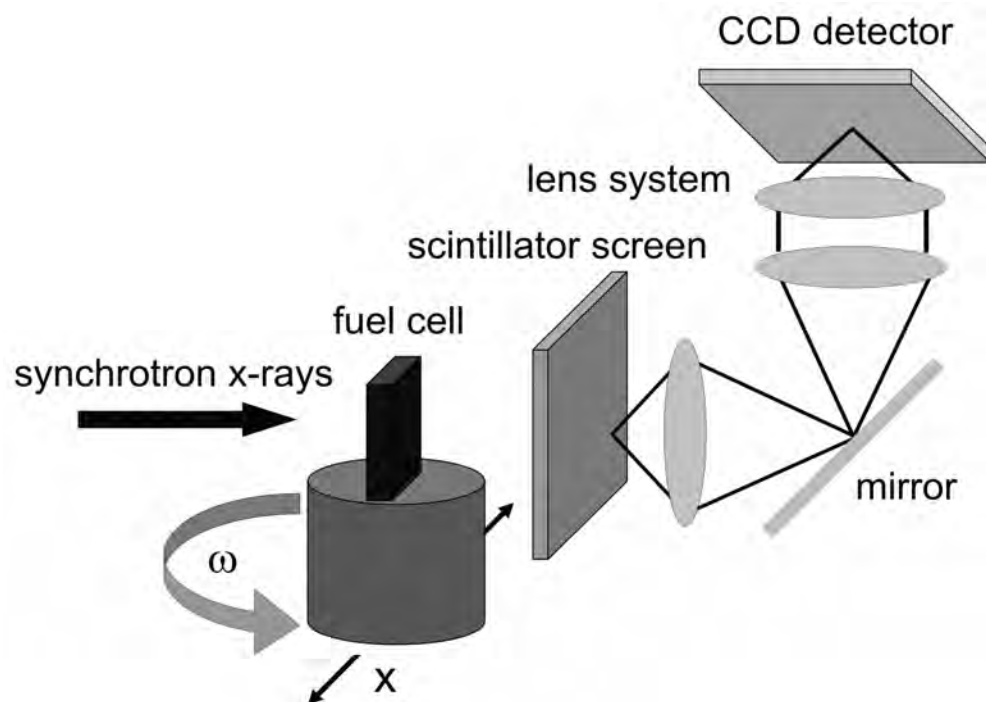


Fig. 2: Schematic drawing of the experimental setup.
85x60mm (600 x 600 DPI)

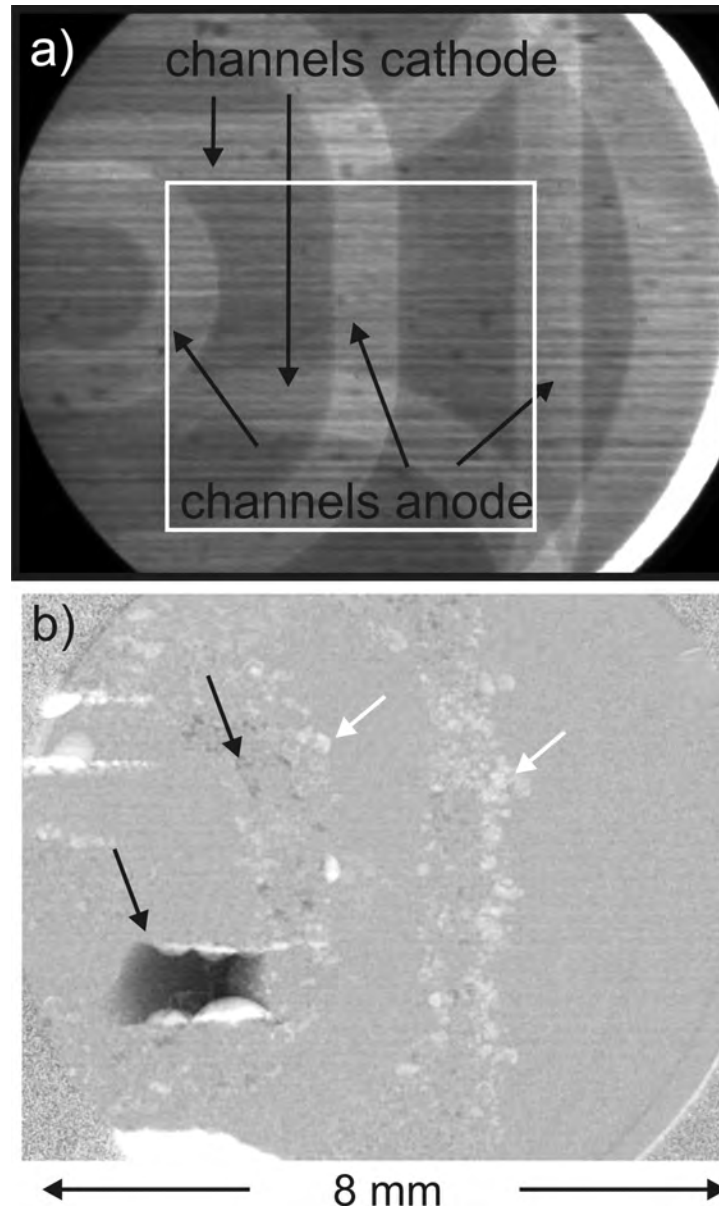


Fig.3: (a) Radiogram as obtained during the experiment. The flow field channels on the cathode and anode side can be seen. (b) A radiogram normalized with respect to a "dry" cell. The white spots in the image can be assigned to water clusters in GDL material and flow field channels. However, the dry cell still contained some residual water that can be identified as black areas in image (b). In this case, a large droplet was located in the anodic flow field channel and was removed after the fuel cell was started (see text for further description). Thus it can be identified as "negative" (black) water accumulation.
85x142mm (600 x 600 DPI)

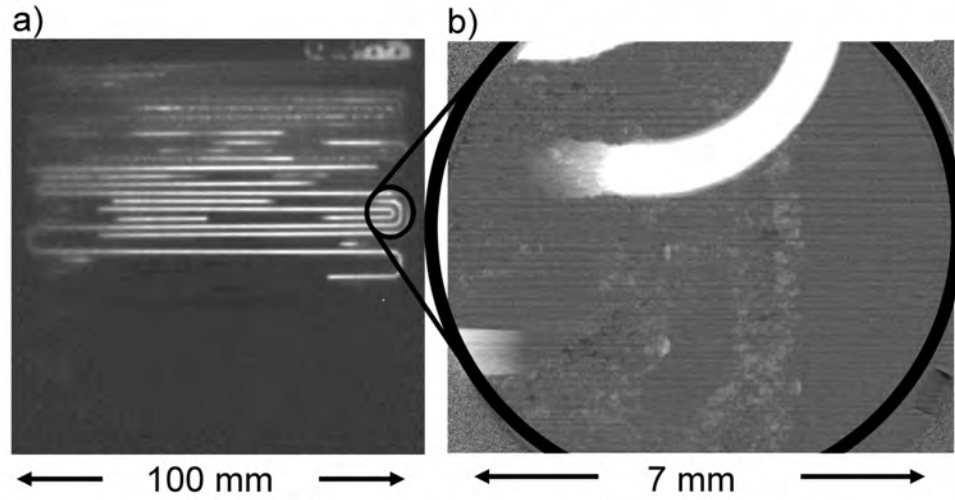


Fig. 4: Complementarity of neutron and synchrotron x-ray radiography: a) Neutron radiogram of the whole active area of a PEM fuel cell and b) synchrotron x-ray radiogram of one part of the same cell with high spatial resolution around a few μm .
85x52mm (600 x 600 DPI)

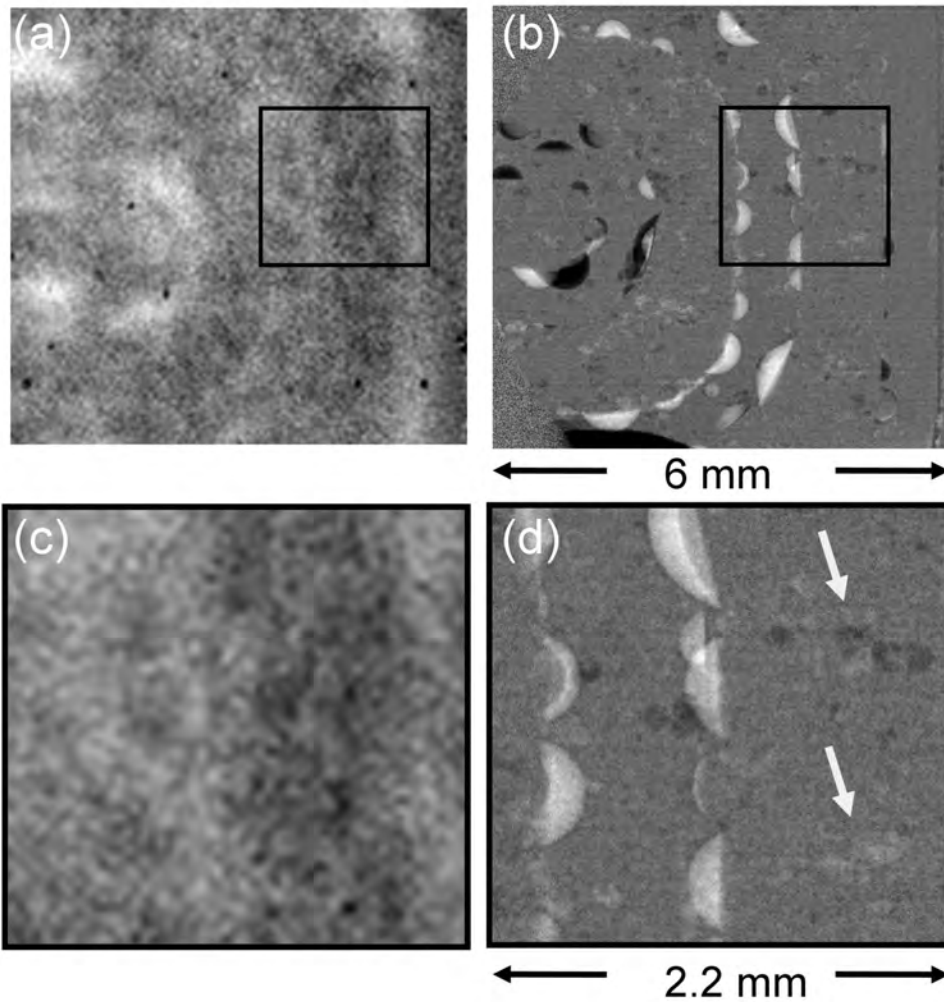


Fig. 5: Comparison of the image qualities obtained with neutron and with synchrotron x-ray radiography for fast measurements with time resolutions around a few seconds. The same location within the same fuel cell was investigated by a) neutron radiography and b) synchrotron x-ray radiography. Corresponding enlargements of the black marked areas in a) and b) are shown in c) and d), respectively.

85x87mm (600 x 600 DPI)

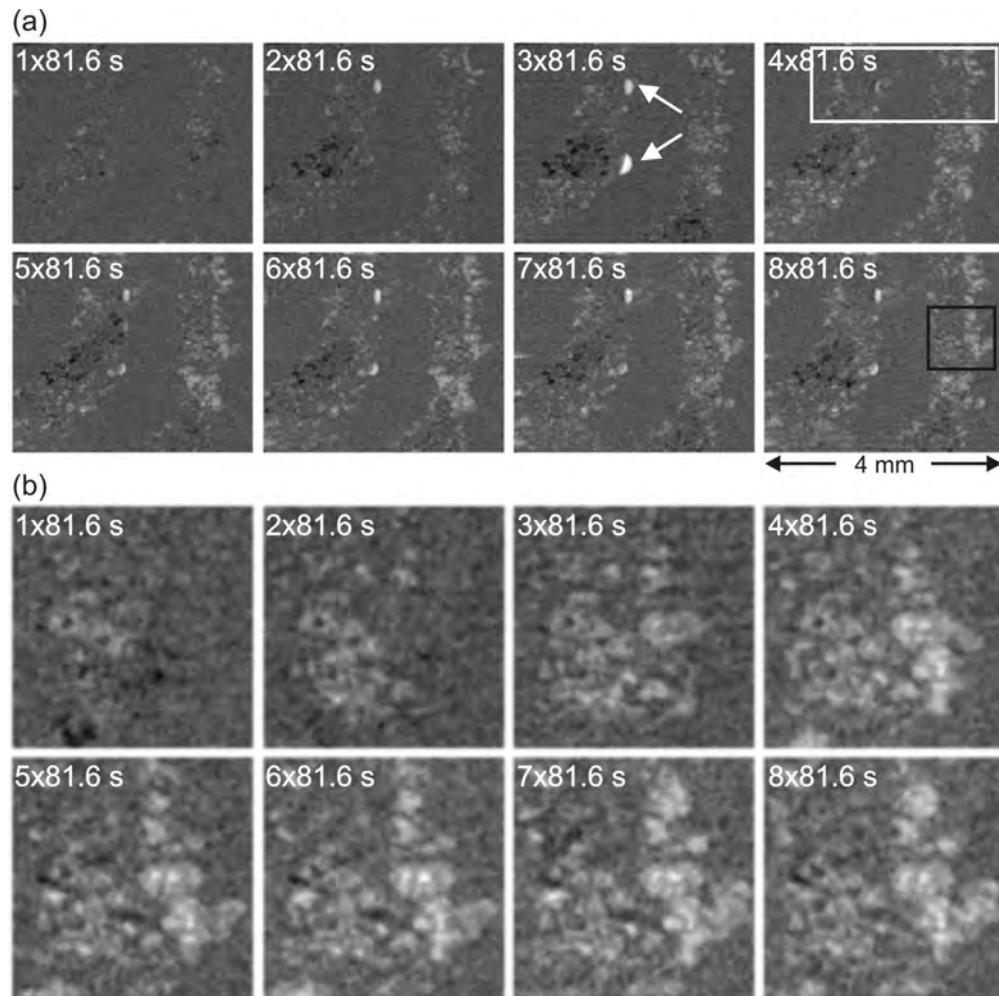


Fig. 6: a) Evolution of liquid water accumulation. The imaged area corresponds to the area marked with a white square in Fig. 3. The time is given in multiples of 81.6 s. The fuel cell was started at an almost dry state. After about 7x81.6 s almost stationary conditions were achieved (the white rectangle denotes the area for the quantification in Fig. 7). b) Corresponding sequence with an enlarged field of view [area marked by a black square in Fig. 6a)].
85x85mm (600 x 600 DPI)

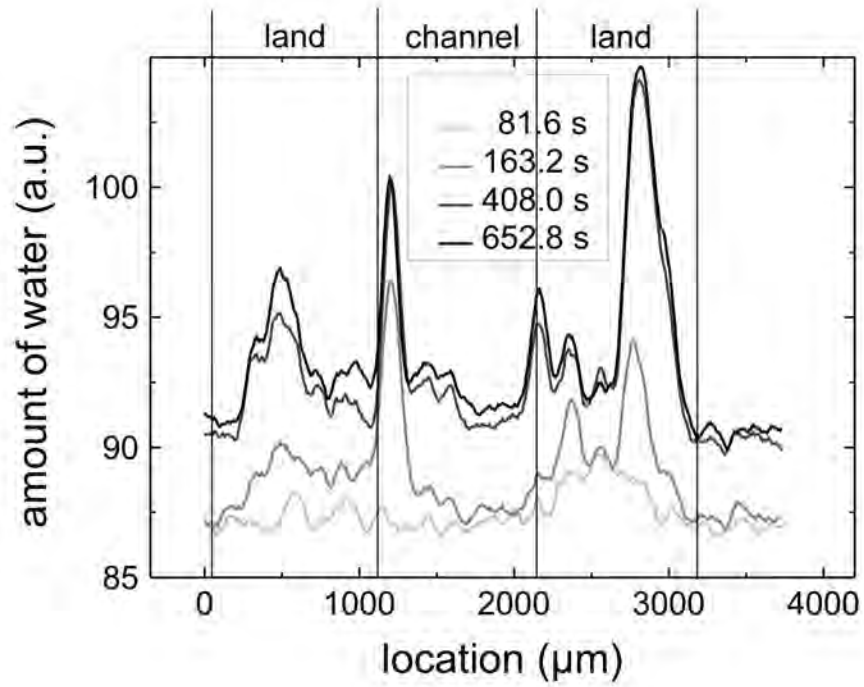


Fig. 7: Quantification of the water distribution along the location marked by a white rectangle in Fig. 6 a) [top right image].
85x67mm (600 x 600 DPI)

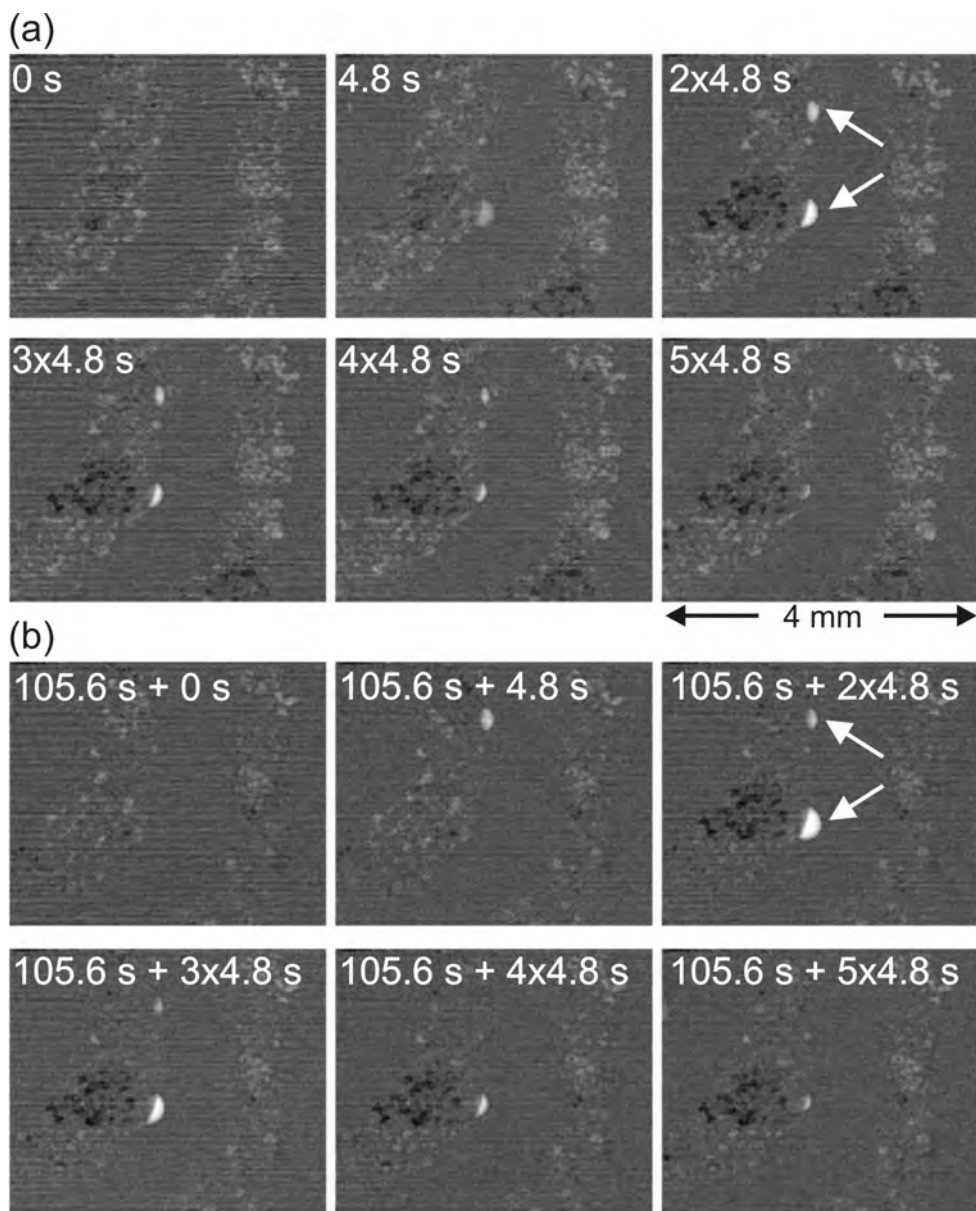


Fig.8: Two sequences showing the eruptive water transport found in Fig. 6 with smaller time steps (4.8s between succeeding images) at the same location. Both sequences show eruptive water expulsion from pores inside the GDL to the cathodic flow field channel. The droplets in the flow field channels are marked by arrows. Sequence b) was measured 105.6 s later. It can be clearly seen that both image series are almost identical, i.e. the eruptive process is periodic.
85x106mm (600 x 600 DPI)

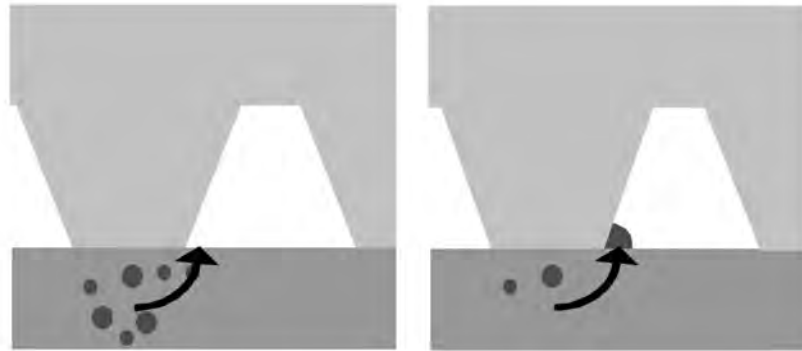


Fig 9: Schematic drawing explaining the eruptive water transport. Water in the GDL is expelled within less than 5 s into the flow field where it forms a droplet.
85x41mm (600 x 600 DPI)

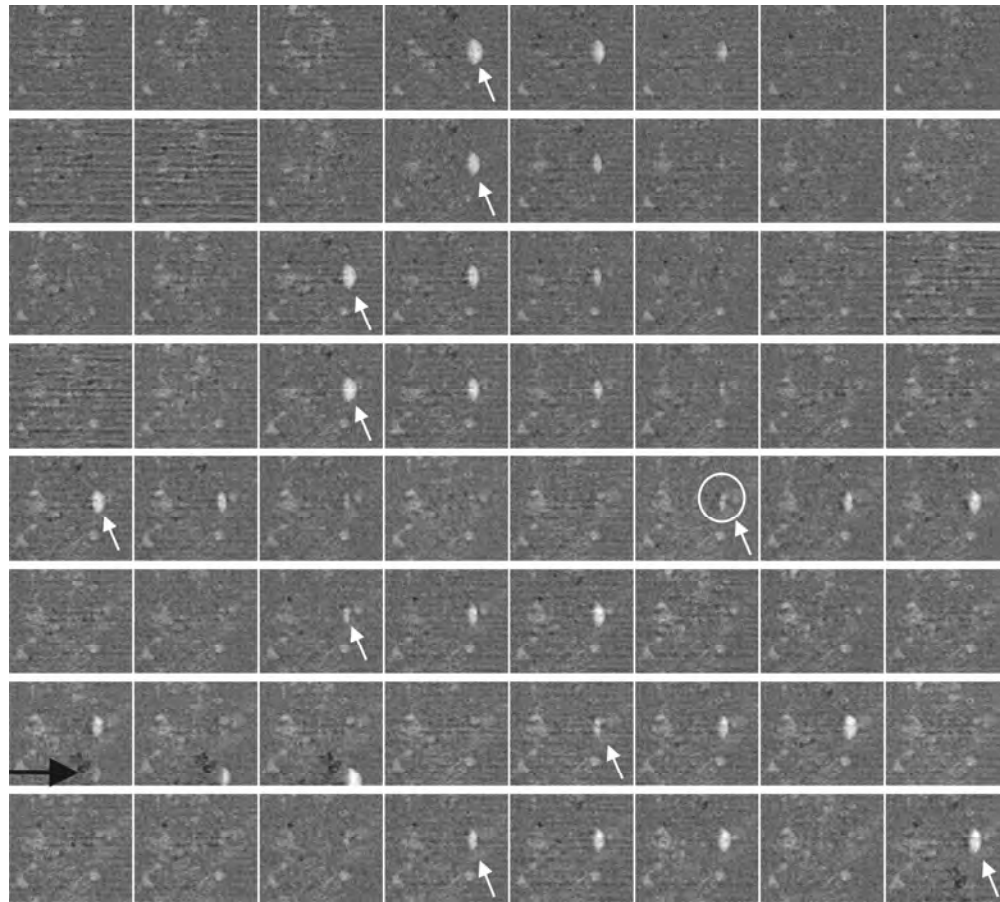


Fig. 10: Eruptive water expulsion from the gas diffusion layer to the cathodic flow field channel: The images show the water distribution in a small area of about $1.4 \times 1.2 \text{ mm}^2$. It is a sequence of succeeding images with a time separation of 4.8 s. At the beginning ($t = 0 \text{ s}$) the cathodic utilization rate was increased from 95 to 97.5 %. This yields an increase in the repetition rate of the eruptive process. After around 200 s, a second transport channel was opened around 0.5 mm below the first channel (location is marked by a black arrow).

169x152mm (600 x 600 DPI)

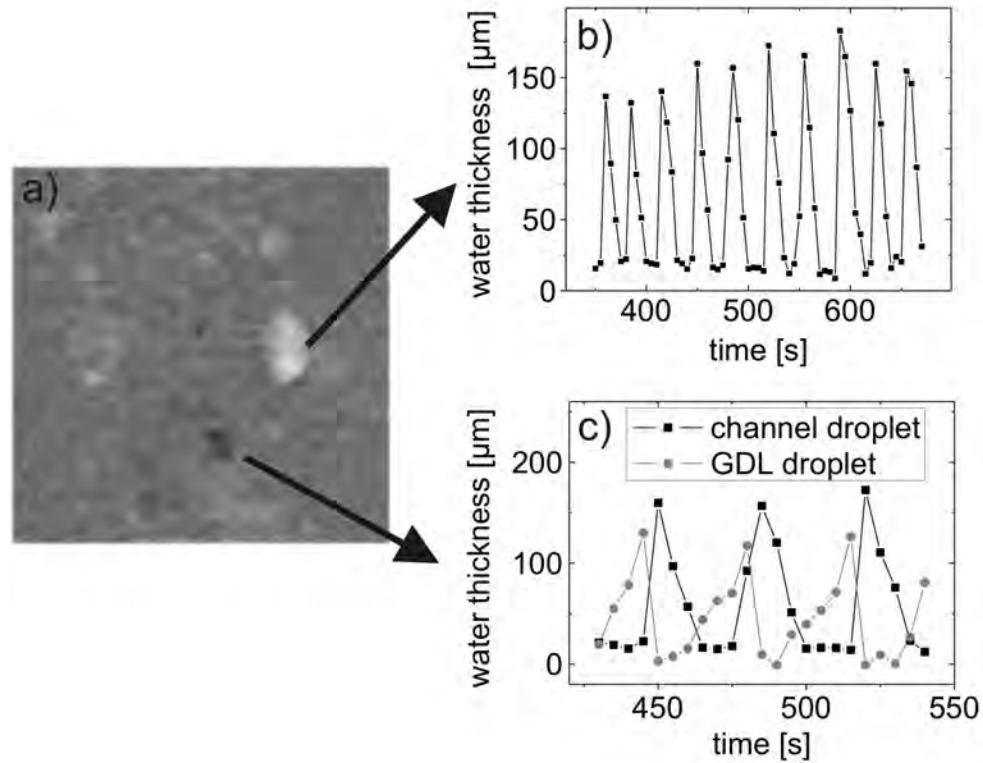


Fig 11: Temporal correlation between water content in the GDL pores and in the corresponding flow field channel (large water droplet). Water accumulations shown in the images in Fig. 10 were quantified for a specific time interval at the two locations marked by arrows. b) amount of water (transmission thickness) at the location of the droplet, c) at a chosen location within the GDL. For comparison, the corresponding water accumulation at the droplet position is also shown in b). The GDL pore is slowly filled until it is emptied very quickly. At the same time the water droplet forms and is evaporated during the next 10 - 15 sec.

85x71mm (600 x 600 DPI)